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71 Applicant: SHELL INTERNATIONALE
RESEARCH MAATSCHAPPIJ B.V.
Carel van Bylandtlaan 30
NL-2596 HR Den Haag(NL)

72 Inventor: Reinalda, Donald
Badhuisweg 3
NL-1031 CM Amsterdam(NL)
Inventor: Kars, Jelte
Vondelingenweg 601
NL-3196 KK Rotterdam(NL)

74 Representative: Aalbers, Onno et al
P.O. Box 302
NL-2501 CH The Hague(NL)

54 Process for the preparation of a catalyst or catalyst precursor suitable for the preparation of hydrocarbons from carbon monoxide and hydrogen, and said catalyst.

57 Process for the preparation of a catalyst or catalyst precursor suitable for the preparation of hydrocarbons from carbon monoxide and hydrogen, wherein a cobalt compound is applied on a porous, inert carrier and the carrier provided with the cobalt compound is dried and calcined forming the catalyst, characterized in that the cobalt compound is cobalt nitrate, and the carrier provided with the cobalt compound is calcined in an atmosphere containing nitrogen oxide at a concentration of at least 20% by volume, taking the water content of the atmosphere not into consideration, catalyst comprising agglomerates of cobalt oxide crystallites distributed over a porous, inert carrier, having an agglomerate size of about 1-10 micrometer, and hydrocarbons prepared.

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PROCESS FOR THE PREPARATION OF A CATALYST OR CATALYST PRECURSOR SUITABLE FOR THE PREPARATION OF HYDROCARBONS FROM CARBON MONOXIDE AND HYDROGEN, AND SAID CATALYST

The present invention relates to a process for the preparation of a catalyst or catalyst precursor suitable for the preparation of hydrocarbons from a mixture of carbon monoxide and hydrogen, and to said catalyst per se.

The preparation of hydrocarbons from a gas mixture comprising carbon monoxide and hydrogen by contacting this mixture at elevated temperatures and pressure with a suitable catalyst, is known in the literature as the Fischer-Tropsch process. Suitable catalysts for this synthesis reaction are amongst others catalysts comprising cobalt supported on a porous, inert carrier. These catalysts are especially suitable for the preparation of heavy paraffinic hydrocarbons. Optionally a noble metal, e.g. ruthenium, may be added. Furthermore, the catalysts preferably contain at least one other metal from Group 4b and/or 6b, preferably chosen from the group consisting of hafnium, zirconium, titanium and chromium. Magnesium, thorium and manganese may also be used.

Impregnation and/or kneading are conventional methods for the incorporation of cobalt and optionally the promoter and other metals into the carrier. For further information reference is made to EP-A-127,220.

The metal loaded carrier is usually dried in order to remove the solvent at temperatures varying from ambient temperature to 200 °C at normal pressure. Thereafter the dried catalyst composition is calcined at temperatures from 200-700 °C, preferably 300-600 °C, in order to remove crystal water and to decompose organic and inorganic compounds to oxides and volatile decomposition products, for instance nitrogen oxide.

Prior to the use of the above-described Fischer Tropsch catalysts, the catalysts have to be activated. This activation is suitably carried out by contacting the catalyst at a temperature between 100 and 600 °C, preferably between 200 and 350 °C, with hydrogen or a hydrogen containing gas.

Further research on the activity and selectivity, especially the C₅ + selectivity, of the catalysts revealed that the selectivity and the activity may be further improved, if during the calcination the metal loaded carrier resides in an atmosphere containing nitrogen oxide.

The present invention, therefore, relates to a process for the preparation of a catalyst or catalyst precursor suitable for the preparation of hydrocarbons from a mixture of carbon monoxide and hydrogen, wherein a cobalt compound is applied on a porous, inert carrier and the carrier provided with the cobalt compound is dried and calcined forming the catalyst, characterized in that the cobalt compound is cobalt nitrate, and the carrier provided with the cobalt compound is calcined in an atmosphere containing nitrogen oxide in a concentration of at least 20% by volume, taking the water content of the atmosphere not into consideration.

Preferably the nitrogen oxide originates from the decomposition of cobalt nitrate, and this decomposition gas is present if during calcination the atmosphere in the calcination furnace is not purged at all, or is purged at a low velocity.

The concentration of the nitrogen oxide during the calcination process is suitably between 25 and 100% by volume, preferably between 40 and 95% by volume, more preferably between 60 and 90% by volume, taking the water content of the atmosphere not into consideration. The concentration of the nitrogen oxide during calcination may be established by measuring the nitrogen oxide concentration in the (dried) off-gas from the calcination process, or by taking samples out of the calcination bed.

The calcination in the presence of nitrogen oxide results in the formation of relatively large agglomerates of cobalt oxide crystallites, and subsequently of relatively large agglomerates of cobalt crystallites after reduction. The relatively large cobalt oxide agglomerates usually have a size of between 1 and 10 micrometer, preferably between 1 and 5 micrometer, more preferably between 1 and 3 micrometer, still more preferably between 1.5 and 2.5 micrometer. Therefore, the invention also relates to a process for the preparation of catalysts suitable for the preparation of hydrocarbons as described hereinbefore, wherein the nitrogen oxide concentration is such that cobalt oxide containing agglomerates are formed having a size of about 1-10 micrometer, preferably between 1 and 5 micrometer, more preferably between 1 and 3 micrometer, still more preferably between 1.5 and 2.5 micrometer, as well as to catalysts having cobalt agglomerates having a size of about 1-10 micrometer, preferably between 1 and 5 micrometer, more preferably between 1 and 3 micrometer, still more preferably between 1.5 and 2.5 micrometer.

The catalysts preferably contain about 3-80 parts by weight cobalt, especially 15-50 parts by weight of cobalt, optionally 0.05-0.5 parts by weight ruthenium, and about 0.1-100 parts by weight of other metal (as per 100 parts by weight carrier), preferably 5-40 parts of zirconium. The porous carrier is preferably a refractory oxide carrier, such as silica, alumina, zirconia, titania and mixtures thereof; preferably silica or

titania, especially silica, is used.

The catalysts or catalyst precursors are preferably used in the form of spherical, cylindrical or lobed particles having a nominal diameter of 0.5-5 mm, preferably 1-2 mm. The carrier particles may be prepared by any conventional method, such as compression, granulation, (hot)pressing or extrusion of powderous carrier material, optionally using a binder material. Carrier spheres, in particular silica containing spheres, are suitably prepared by means of the "oil-drop" method, wherein spheres are formed from drops of silica precursor and an acid solidifying when falling in an oil bath, or by means of the "sol-gel" method. Alumina based carriers are preferably made by extrusion or by the above described "oil-drop" method.

The preparation of hydrocarbons from a mixture of carbon monoxide and hydrogen, using the catalyst according to the invention is preferably carried out at a temperature of 100-500 °C, at a total pressure of 1-200 bar absolute and a space velocity of 200-20,000 m³ (STP) gaseous feed/m³ reaction zone/hour. Preferred process conditions for the preparation of hydrocarbons include a temperature from 150-300 °C, more preferably 180-230 °C, a pressure of 5-100 bar absolute, more preferably 15-30 bar, and a space velocity of 500-5,000 m³ (STP) gaseous feed/m³ reaction zone/hour. The term "STP" used herein means standard temperature (of 0 °C) and pressure (1 bar absolute). The gaseous feed preferably has a hydrogen/carbon monoxide ratio of 0.4-4, more preferably 0.8-2.5, still more preferably 1.0-1.5.

The invention further relates to a process for the preparation of hydrocarbons by catalytic reaction of carbon monoxide and hydrogen comprising the use of a catalyst as described hereinbefore.

The invention will be illustrated hereafter by a practical example of the preparative process of the catalyst and of the process for the preparation of hydrocarbons using this catalyst.

Example 1

On the surface of a silica carrier particles of zirconia are deposited. Then the zirconia impregnated carrier particles are impregnated with an aqueous solution of cobalt nitrate. The dried particles are divided into two portions (A and B). Sample A is dried in a laboratory rotating film evaporator, wherein heat of evaporation is supplied by an oil bath (200 °C) and transferred via the wall of the rotating flask to the impregnated particles (simulating a rotary kiln drier). Air (25 °C) is used as a purge stream to remove the vapours.

Sample B is dried using hot gas in a vibrating bed configuration wherein heat of evaporation is supplied by the gas (25 °C; simulating a belt drier).

Each catalyst sample (A and B) is divided in two equal parts. The first parts (A-S and B-S) are calcined during 1 hour at 500 °C in a stationary oven.

The second parts of the dried samples (A-T and B-T) are calcined in a standard fixed bed configuration using an air stream (GHSV of 5,000 Nl/1.h), resulting in a low nitrogen oxide (NO_x) partial pressure in the catalyst bed to be calcined. The nitrogen oxide partial pressure under these conditions is lower than 2% by volume.

Example 2

The four catalyst samples (A-S, B-S, A-T and B-T) are tested for their catalytic activity in the preparation of hydrocarbons from a mixture of carbon monoxide and hydrogen.

Each catalyst sample (comprising 34 pbw Co₃O₄, 16 pbw ZrO₂ and 100 pbw SiO₂) is reduced (260 °C, 3 bar (absolute), 6,000 GHSV), in a gas stream with an increasing hydrogen concentration (1-100%).

The test conditions are as follows: pressure 21 bar (absolute), 800 GHSV, hydrogen/carbon monoxide ratio in the feed = 2.

The results are shown in the following table:

Catalyst	A-S	B-S	A-T	B-T
Performance at run hour 200				
Temperature, °C	195	195	205	205
STY, gC ₁ +, l ⁻¹ , h ⁻¹	100	100	100	100
C ₅ + selectivity, %w on C ₁ +	76/79	75	75	76

From this table it is apparent that at the same standard yield, adjusted to 100 gC₁ +, l⁻¹, h⁻¹, with the catalysts calcined according to the invention, comprising the agglomerates of cobalt crystallites, the same yield can be obtained at lower temperatures. At these lower temperatures the occurrence of side reactions is much lower, whereas less iso-hydrocarbons are formed.

Claims

1. Process for the preparation of a catalyst or catalyst precursor suitable for the preparation of hydrocarbons from a mixture of carbon monoxide and hydrogen, wherein a cobalt compound is applied on a porous, inert carrier and the carrier provided with the cobalt compound is dried and calcined forming the catalyst, characterized in that the cobalt compound is cobalt nitrate, and the carrier provided with the cobalt compound is calcined in an atmosphere containing nitrogen oxide in a concentration of at least 20% by volume, taking the water content of the atmosphere not into consideration.
2. Process as claimed in claim 1, wherein the concentration of nitrogen oxide is between about 25 and 100% by volume.
3. Process as claimed in claim 1 or 2, wherein the concentration of nitrogen oxide is between about 40 and 95% by volume.
4. Process as claimed in claims 1-3, wherein the concentration of nitrogen oxide is between about 60 and 90% by volume.
5. Process as claimed in claims 1-4, wherein the nitrogen oxide is at least partly formed by the decomposition of the nitrate-salt.
6. Process as claimed in claims 1-5, wherein the nitrogen oxide concentration is such that cobalt oxide containing agglomerates are formed, having a size of about 1-10 micrometer, preferably 1-5 micrometer.
7. Process as claimed in claim 6, wherein the agglomerate size is about 1-3 micrometer, preferably 1.5-2.5 micrometer.
8. Process as claimed in claims 1-7, wherein the calcination temperature is 200-700 °C, preferably 300-600 °C.
9. Catalyst suitable for the preparation of hydrocarbons from a mixture of carbon monoxide and hydrogen after activation, comprising agglomerates of cobalt oxide crystallites distributed over a porous, inert carrier, having an agglomerate size of about 1-10 micrometer, preferably 1-5 micrometer, more preferably about 1-3 micrometer, especially 1.5-2.5 micrometer.
10. Catalyst as claimed in claim 9, wherein the carrier is selected from the group consisting of silica, alumina, zirconia, titania and/or mixtures thereof, preferably silica.